

COMSOL Conference 2015 Boston

Session: Optimization and Simulation Methods

Boston Marriott Newton
Boston, MA

Commonwealth Ballroom 1
1:00 PM – 2:30 PM

October 8, 2015

Moderator : Jeffrey Fong

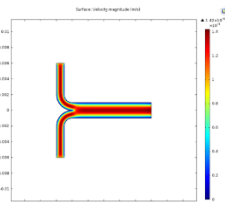
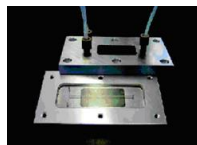
COMSOL
CONFERENCE
2015

COMSOL
CONFERENCE
2015

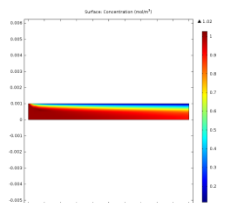
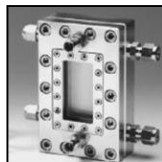
Novel Approach for Teaching Microchemical Systems Analysis to Chemical Engineering Students Using Graphical User Interfaces (GUIs)

Tee-

Micromixer



Microreactor



Anuradha Nagaraj

Department of Environmental Engineering

Anoop Uchagawkar & Patrick L. Mills*

Department of Chemical & Natural Gas Engineering

Texas A & M University-Kingsville

Kingsville, TX 78363-8202 USA

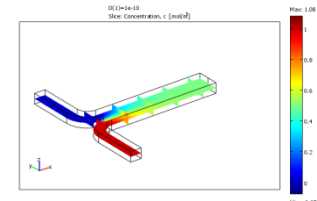
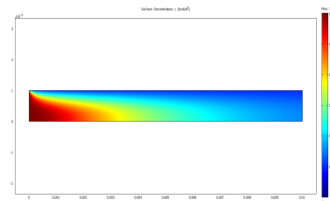
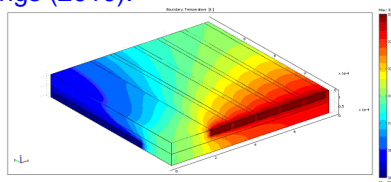
*Patrick.Mills@tamuk.edu



Background

- Next generation technologies must be developed that potentially change the chemical plants and process engineering giving rise to safe, compact, flexible, eco-friendly, energy efficient processes and plants.
- Traditional educational curriculum provide engineering students with a spectrum of theoretical knowledge, but generally provide limited exposure to more advanced technologies.
- Utilization of process simulators and design tools allow engineering students to gain useful exposure to advanced technologies.
- Microprocess systems is one of the key emerging technologies with applications ranging from discovery research through commercial processes.
- This technology was introduced as part of the NSF funded web-based learning resource called *Interlinked Curriculum Components* (ICCs) to educate undergraduate students*.

*P.L. Mills *et al.*, Development Of A Web Based Self Teaching And Module For Chemical Engineering Microchemical Systems, American Society for Engineering Education Conference Proceedings (2010).



Microprocess Systems ICC

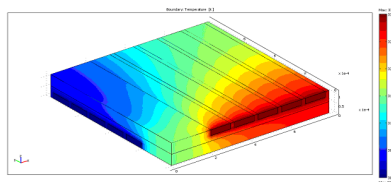
Objectives:

1. Introduce MEMS as applied to microreaction systems.
2. Broaden exposure to multi-scale type of analysis.
3. Strengthen understanding & insight into system behavior.

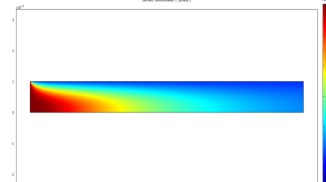
Focus Areas:

- MEMS & microreactors → Components, materials, & fabrication processes
- Microfluidics → Fluid mechanics at the microscale
- Transport phenomena → Coupled momentum & energy transport
- Transport-kinetic effects → Coupled momentum, energy, & species transport
- Device & system design → Microprocess component & system performance

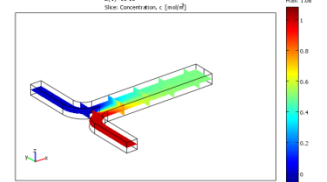
Micro Heat Exchanger



Microchannel Reactor



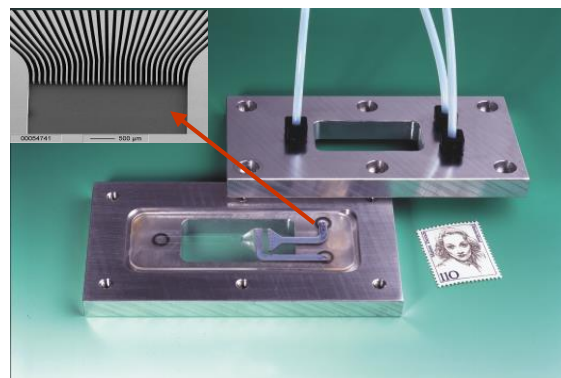
Micro Fluid Mixer



Microreactors & Microprocess Components Fabricated from Glass & Metal



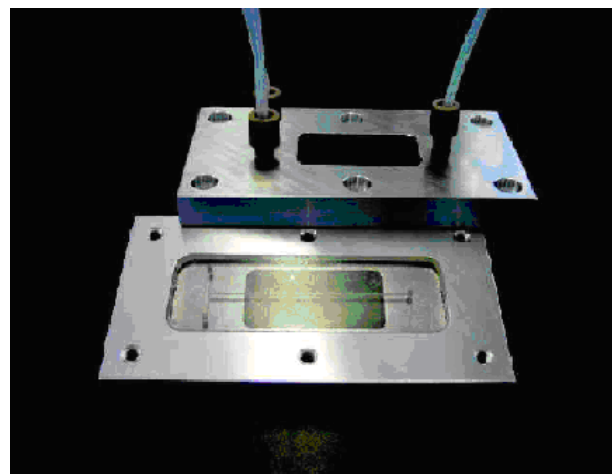
Falling Film Gas-liquid
Microreactor



Interdigital Micromixer
for Two-phase Systems



Cross-flow Heat
Exchanger



Tee-Micromixer (Glass)

Microchannel vs Conventional Reactors

-Typical Ranges for Design Parameters-

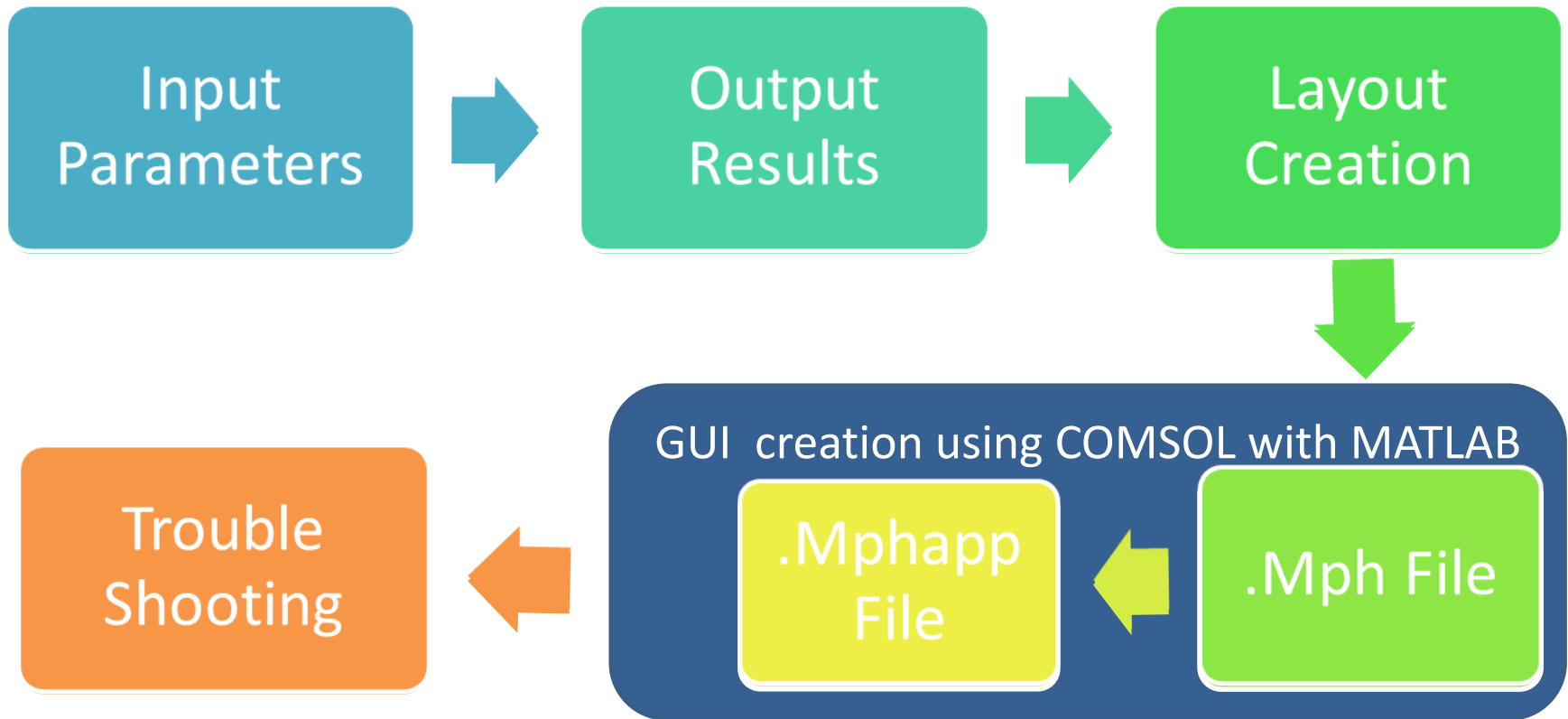
Design Parameter	Microchannel Reactor	Conventional Reactor
Internal volume	1-1000 μL	100 ml-30,000 L
Surface Area/Volume	10,000-50,000 m^2/m^3	100-1000 m^2/m^3
Heat transfer coeff.	10-25,000 $\text{kW}/\text{m}^2/\text{K}$	17-25 $\text{kW}/\text{m}^2/\text{K}$
Film thickness	$\sim 25 \mu\text{L}$	$\sim 250 \mu\text{L}$
Mixing time	$< 1 \text{ sec}$	$> 1 \text{ sec}$
Power input	10 X less	X

Angew. Chem. Int. Ed. 43,406,2004

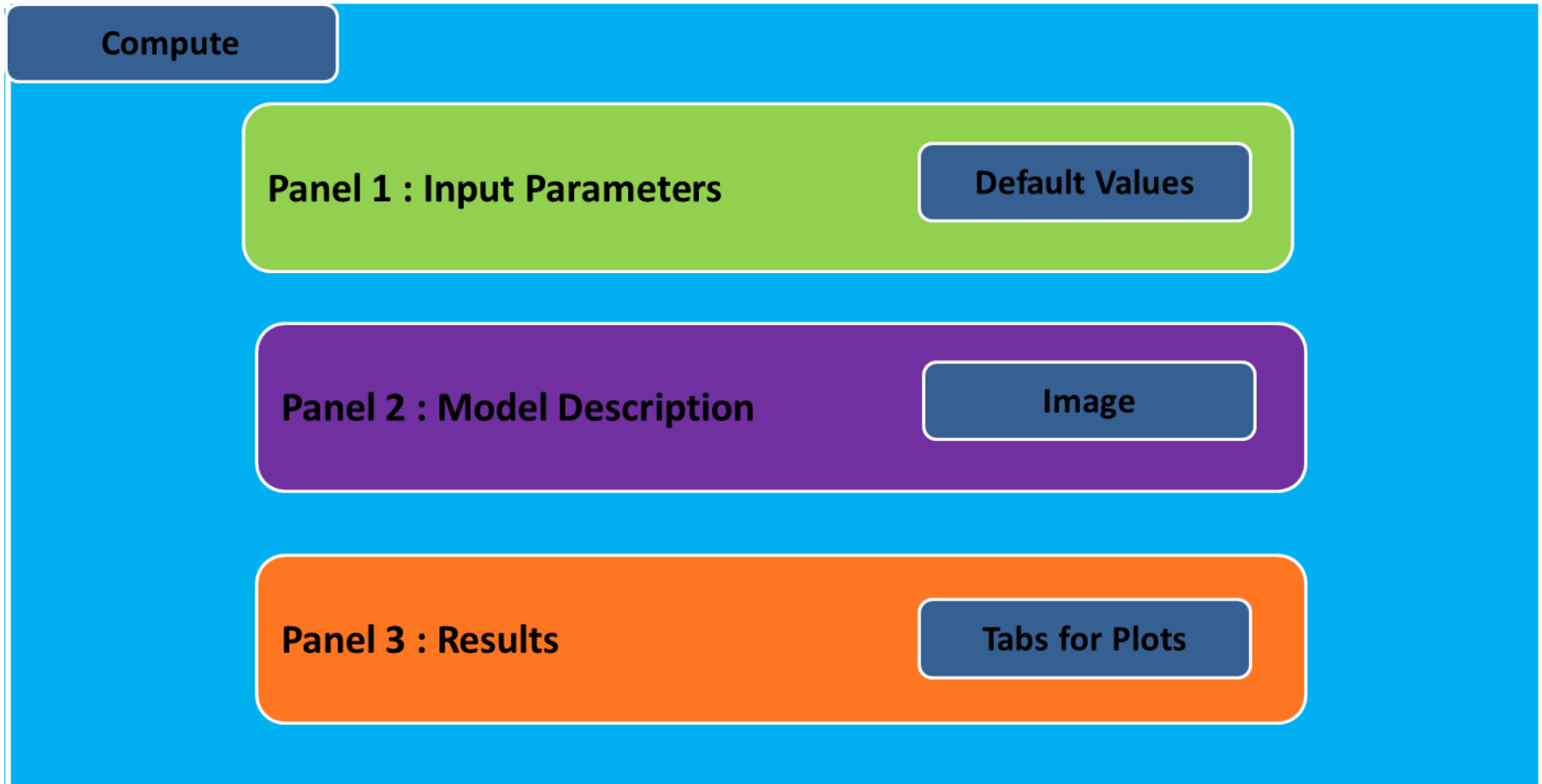
Graphical User Interface (GUI)

- Readily allows users to modify key system parameters and to obtain graphical results.
- Advantages of GUI's in COMSOL
 - Reduces the complications with model development
 - Simplifies assigning boundary conditions
 - Allows visualization of various model parameters
 - Improves understanding of model physics *vs* details associated with the model development

Steps Involved in GUI Creation



Example of Typical GUI Layout



Catalytic Wall Reactor

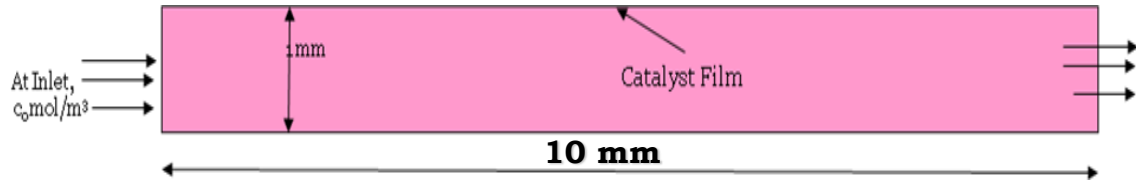
Objective

Illustrate the interactions between fluid transport and chemical kinetics for a steady-state model of a simple wall-microreactor with a first-order reaction

Channel Dimensions

Length: 10 mm

Height: 1 mm



Input Parameters

- Fluid density & fluid viscosity
- Inlet solute concentrations
- Two choices for boundary conditions
 - Specified inlet velocity & outlet pressure
 - Specified inlet & outlet pressure

Chemistry



Reaction Rate

$$-r_A = k C_A$$

Model Equations and Kinetics

Model Equations:

Momentum Transport Equations

x- direction:

$$\rho \left[\frac{\partial u_x}{\partial t} \right] - \eta \left[\frac{\partial^2 u_x}{\partial x^2} + \frac{\partial^2 u_x}{\partial y^2} \right] + \rho \left[u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} \right] + \frac{\partial p}{\partial x} = F_x$$

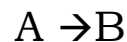
y-direction:

$$\rho \left[\frac{\partial u_y}{\partial t} \right] - \eta \left[\frac{\partial^2 u_y}{\partial x^2} + \frac{\partial^2 u_y}{\partial y^2} \right] + \rho \left[u_x \frac{\partial u_y}{\partial x} + u_y \frac{\partial u_y}{\partial y} \right] + \frac{\partial p}{\partial y} = F_y$$

Convection - Diffusion Equation:

$$D \left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} \right) - \left(u_x \frac{\partial c}{\partial x} + u_y \frac{\partial c}{\partial y} \right) + v_i R = \frac{\partial c}{\partial t}$$

Reaction Kinetics:



$$\text{rate, } r_A = k C_A$$

Catalytic Wall Microreactor Results

Catalytic Wall Reactor

Input

Parameter	Value	Units
Rate Constant	1.5	1/s
Diffusion Coefficient of A	1e-7	m ² /s
Diffusion Coefficient of B	0.5e-7	m ² /s
Concentration of A	1	mol/m ³
Concentration of B	0	mol/m ³
Density	1e3	kg/m ³
Dynamic Viscosity	1e-3	kg/(m·s)
Inlet Pressure	0.1	Pa
Outlet Pressure	0	Pa

Reactor Description

Inlet: A → **Catalytic Wall** (A → B) → Outlet: A, B

Model Description

Results Panel

COMSOL MULTIPHYSICS

Velocity | Pressure | Concentration of Specie A | Concentration of Specie B **Tabs**

Catalytic Wall Reactor

Input

Parameter	Value	Units
Rate Constant	1.5	1/s
Diffusion Coefficient of A	1e-7	m ² /s
Diffusion Coefficient of B	0.5e-7	m ² /s
Concentration of A	1	mol/m ³
Concentration of B	0	mol/m ³
Density	1e3	kg/m ³
Dynamic Viscosity	1e-3	kg/(m·s)
Inlet Pressure	0.1	Pa
Outlet Pressure	0	Pa

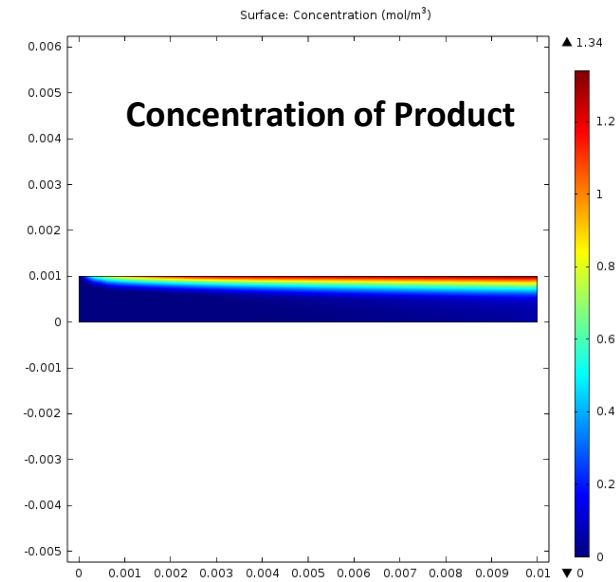
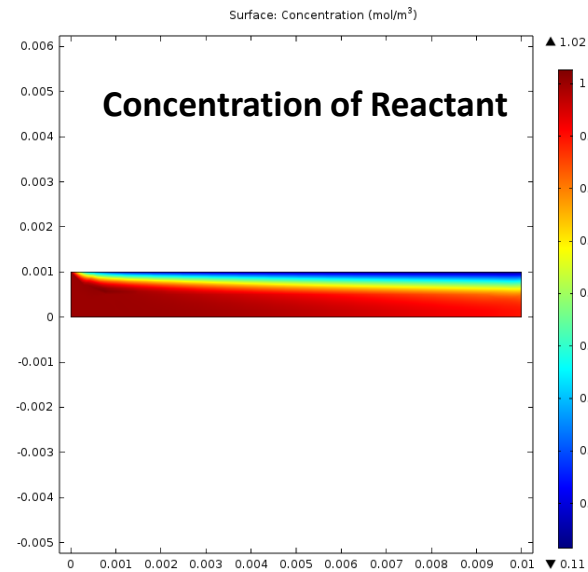
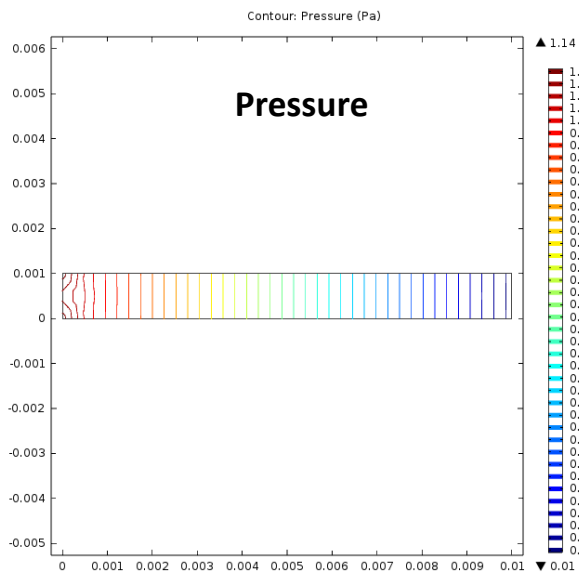
Reactor Description

Inlet: A → **Catalytic Wall** (A → B) → Outlet: A, B

COMSOL MULTIPHYSICS

Velocity | Pressure | Concentration of Specie A | Concentration of Specie B

Surface: Velocity magnitude (m/s)



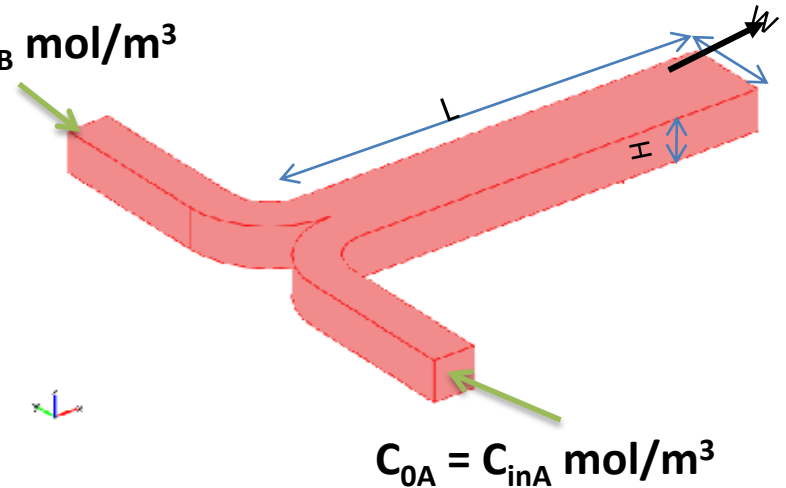
T-Micromixer

Objective

Illustrate the interactions between fluid transport and chemical kinetics for a steady-state model of a simple T-microreactor with a second-order reaction

Channel Dimensions

Length :	10 mm	$C_{0B} = C_{inB}$ mol/m ³
Width :	1 mm	
Height :	1 mm	
Circular Baffles Diameter	0.3 mm	



Input Parameters

- Fluid density & fluid viscosity
- Inlet solute concentration
- Two choices for boundary conditions
 - Specified inlet velocity & outlet pressure
 - Specified inlet & outlet pressure

Model Equations and Kinetics

Model Equations:

Momentum Transport Equations

$$\text{x-direction: } \rho \left[\frac{\partial u_x}{\partial t} \right] - \eta \left[\frac{\partial^2 u_x}{\partial x^2} + \frac{\partial^2 u_x}{\partial y^2} + \frac{\partial^2 u_x}{\partial z^2} \right] + \rho \left[u_x \frac{\partial u_x}{\partial x} + u_y \frac{\partial u_x}{\partial y} + u_z \frac{\partial u_x}{\partial z} \right] + \frac{\partial p}{\partial x} = 0$$

$$\text{y-direction: } \rho \left[\frac{\partial u_y}{\partial t} \right] - \eta \left[\frac{\partial^2 u_y}{\partial x^2} + \frac{\partial^2 u_y}{\partial y^2} + \frac{\partial^2 u_y}{\partial z^2} \right] + \rho \left[u_x \frac{\partial u_y}{\partial x} + u_y \frac{\partial u_y}{\partial y} + u_z \frac{\partial u_y}{\partial z} \right] + \frac{\partial p}{\partial y} = 0$$

$$\text{z-direction: } \rho \left[\frac{\partial u_z}{\partial t} \right] - \eta \left[\frac{\partial^2 u_z}{\partial x^2} + \frac{\partial^2 u_z}{\partial y^2} + \frac{\partial^2 u_z}{\partial z^2} \right] + \rho \left[u_x \frac{\partial u_z}{\partial x} + u_y \frac{\partial u_z}{\partial y} + u_z \frac{\partial u_z}{\partial z} \right] + \frac{\partial p}{\partial z} = 0$$

Convection - Diffusion Equation:

$$D \left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} + \frac{\partial^2 c}{\partial z^2} \right) - \left(u_x \frac{\partial c}{\partial x} + u_y \frac{\partial c}{\partial y} + u_z \frac{\partial c}{\partial z} \right) + v_i R = \frac{\partial c}{\partial t}$$

Parameter Estimation:

$$\text{Mixing Effectiveness } \tau = \frac{\tau_v}{\tau_D} = \frac{DL}{u_{avg} * W^2}$$

where ρ is the fluid density, η is the fluid viscosity, p is the fluid pressure, D is diffusivity, c is concentration, u_{avg} is average velocity and L, W, H are duct dimensions

Regular T-Micromixer

T-Micromixer

Input

Parameter	Value	Units
Density	1000	kg/m ³
Viscosity	1e-3	Pa·s
Diffusivity	1e-4	m ² /s
Concentration	1	mol/m ³
Initial Velocity	1e-3	m/s

Model Description

$C_{A0} = 0 \text{ mol/m}^3$

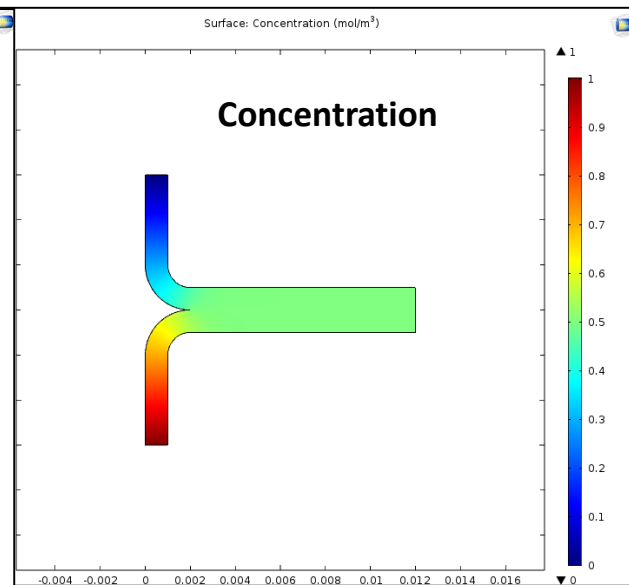
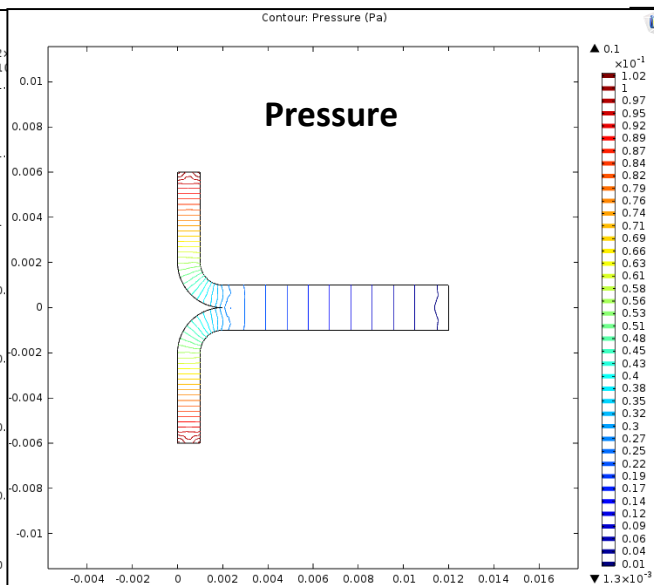
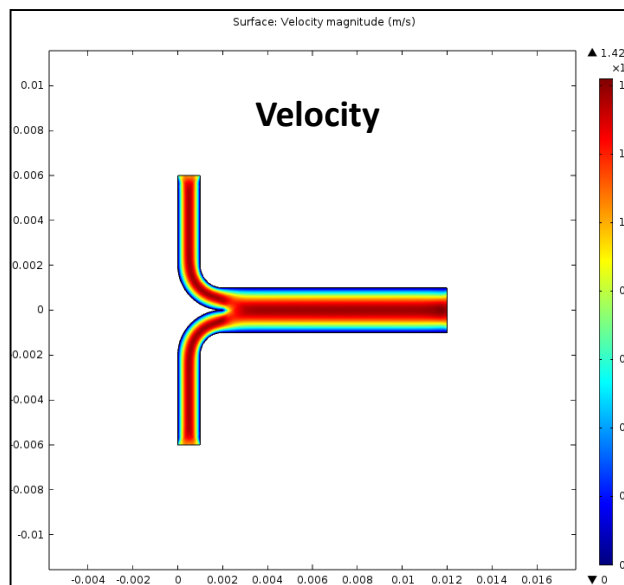
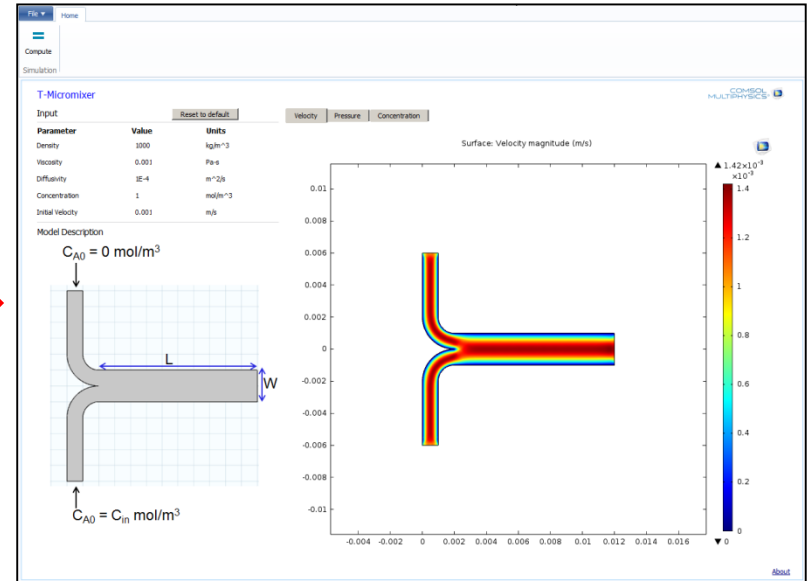
$C_{A0} = C_{in} \text{ mol/m}^3$

Model Description

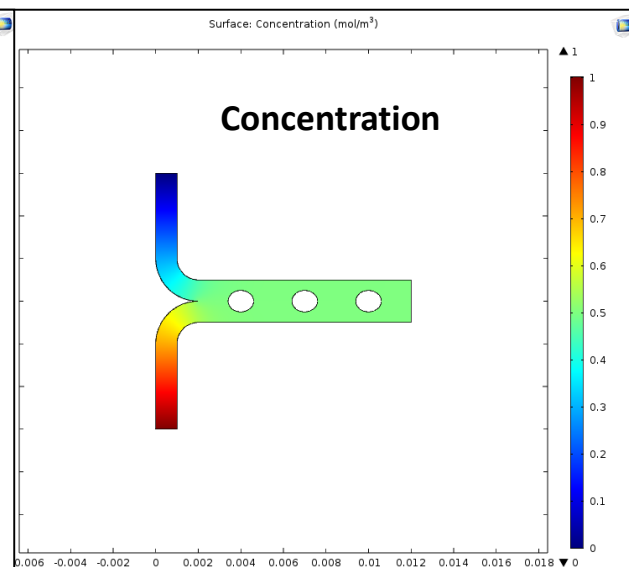
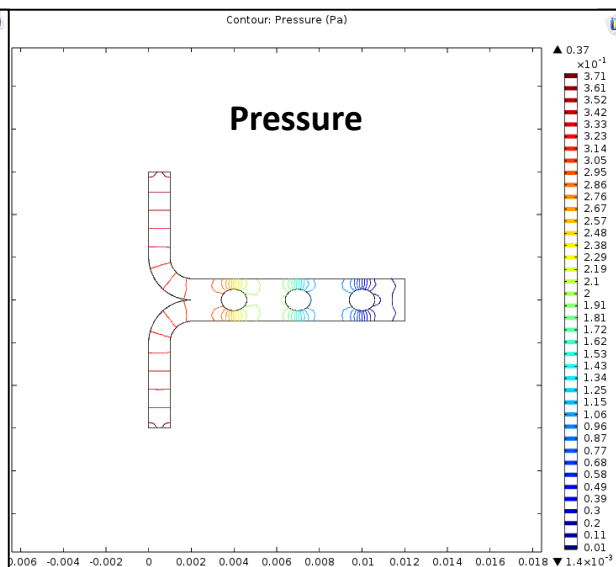
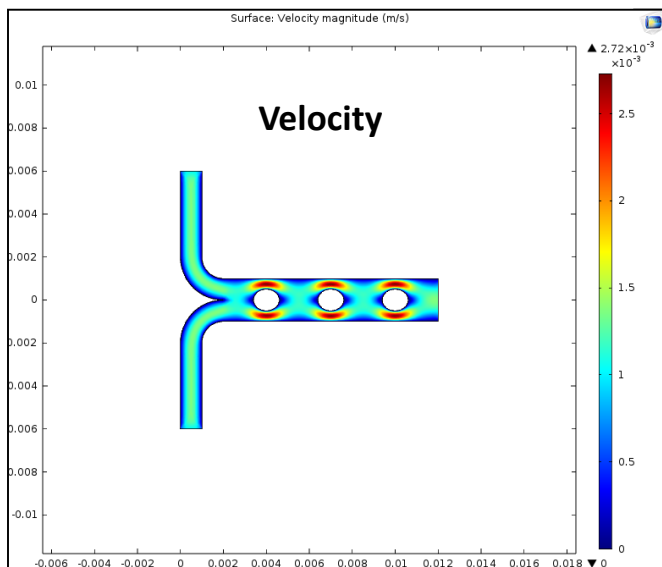
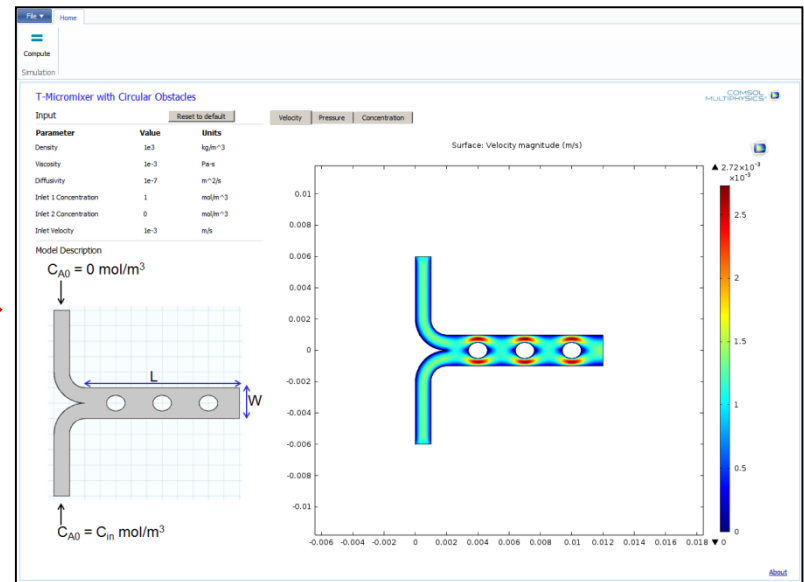
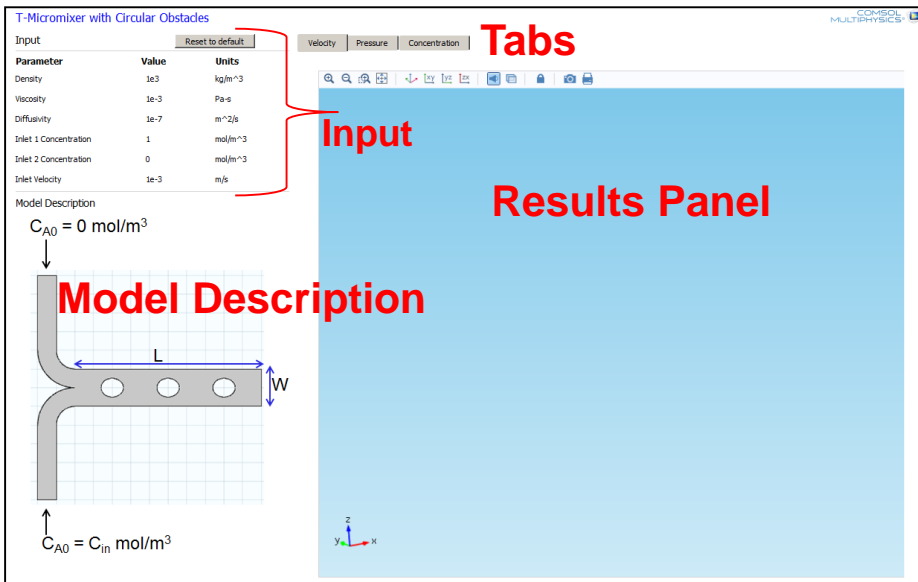
Results Panel

Input

Velocity | **Pressure** | **Concentration** | **Tabs**



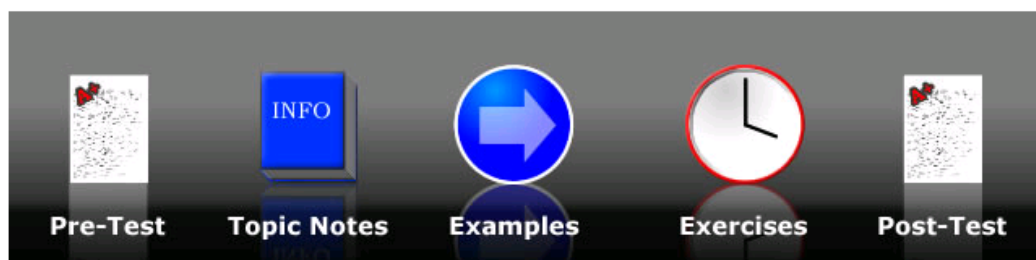
T-Micromixer with Circular Baffles



Conclusions

- COMSOL Multiphysics provides a powerful numerical platform where various models for *microchemical process technology* components can be readily created for both education and research.
- This modeling tool allows chemical engineering students to focus on understanding the *effects of various system design and operational parameters* instead of coding and numerical method debugging.
- The GUIs enable students to readily study the *effect of various design parameters*.
- These applications reduces the *complexity* of model setup and computational time and emphasize understanding of multiphysics in multi-dimensions.
- This approach helps students to understand complex chemical systems using an *interactive approach* vs laborious manual calculations or using other software tools.

Additional Supporting Documentation



Introduction

In this section, you will learn basic principles of flow regimes, and the basic knowledge of simulating models in microchemical systems.

Learning objectives (bold words correspond to indicators in Bloom's taxonomy)

1. You will be able to **define** the terms in the table below.

flow rate	viscosity
Reynolds number	Knudsen number
flow regime	Navier-Stokes equation
newtonian fluid	non-newtonian fluid
boundary settings	subdomain settings

2. You will be able to **create** a concept map that demonstrates the relationships among the terms defined in Objective (1).
3. You will be able to **explain** the difference between
 - conventional flow and micro-scale flow
 - Newtonian fluids and Non-newtonian fluids
 and **give examples** of each.
4. **Learn** more about the effect of subdomain settings and boundary settings on the given geometrical figure.
5. **Become more confident** to simulate various complicated models related to fluid mechanics.



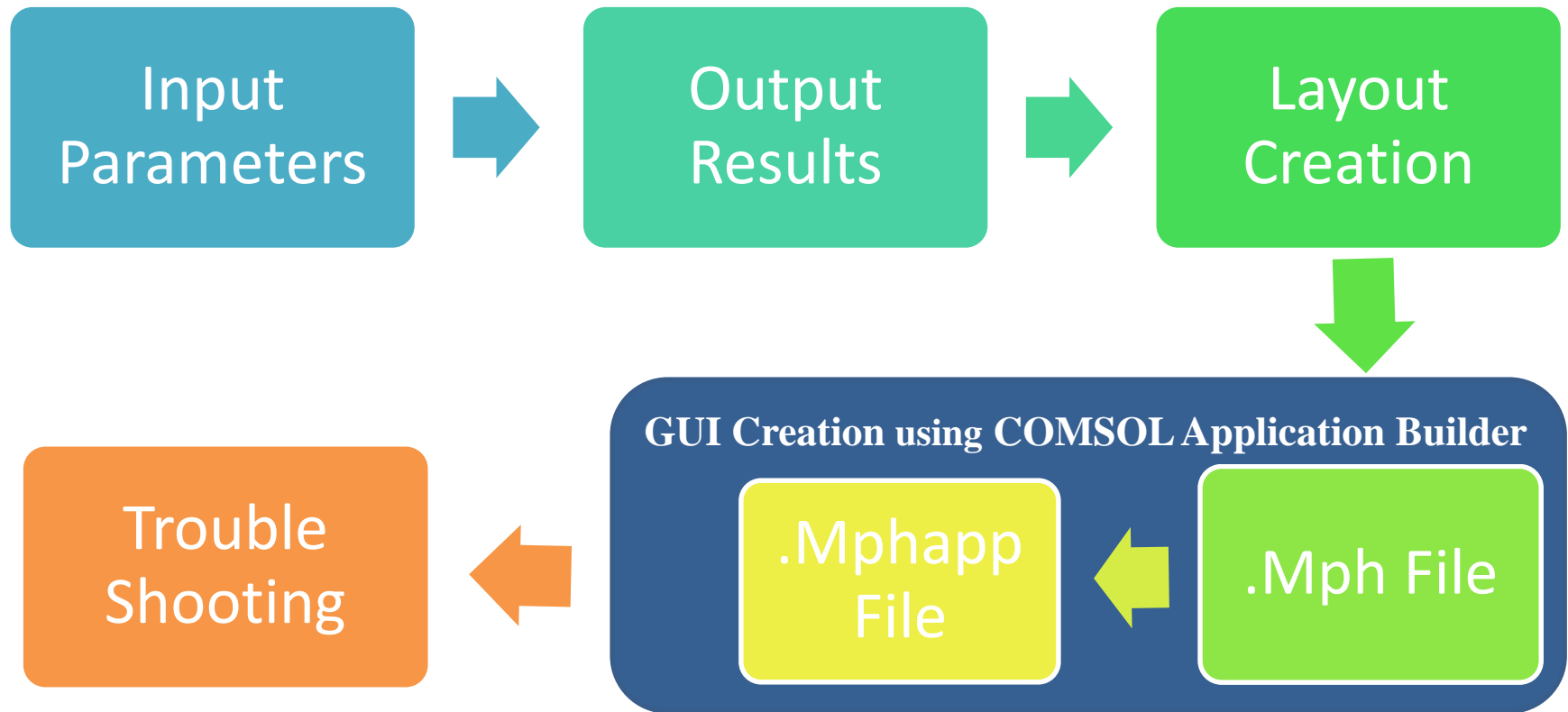
Main Template for an ICC Module

- Provides topical overview on a given subject.
- Directs user to subsections
 - Pre test
 - Topic notes
 - Examples
 - Exercises
 - Post assessment
- Same format for all ICC's
- Navigation bar with buttons provides links to web pages
- Based on *Dreamweaver* and *Flash 8* software tools.

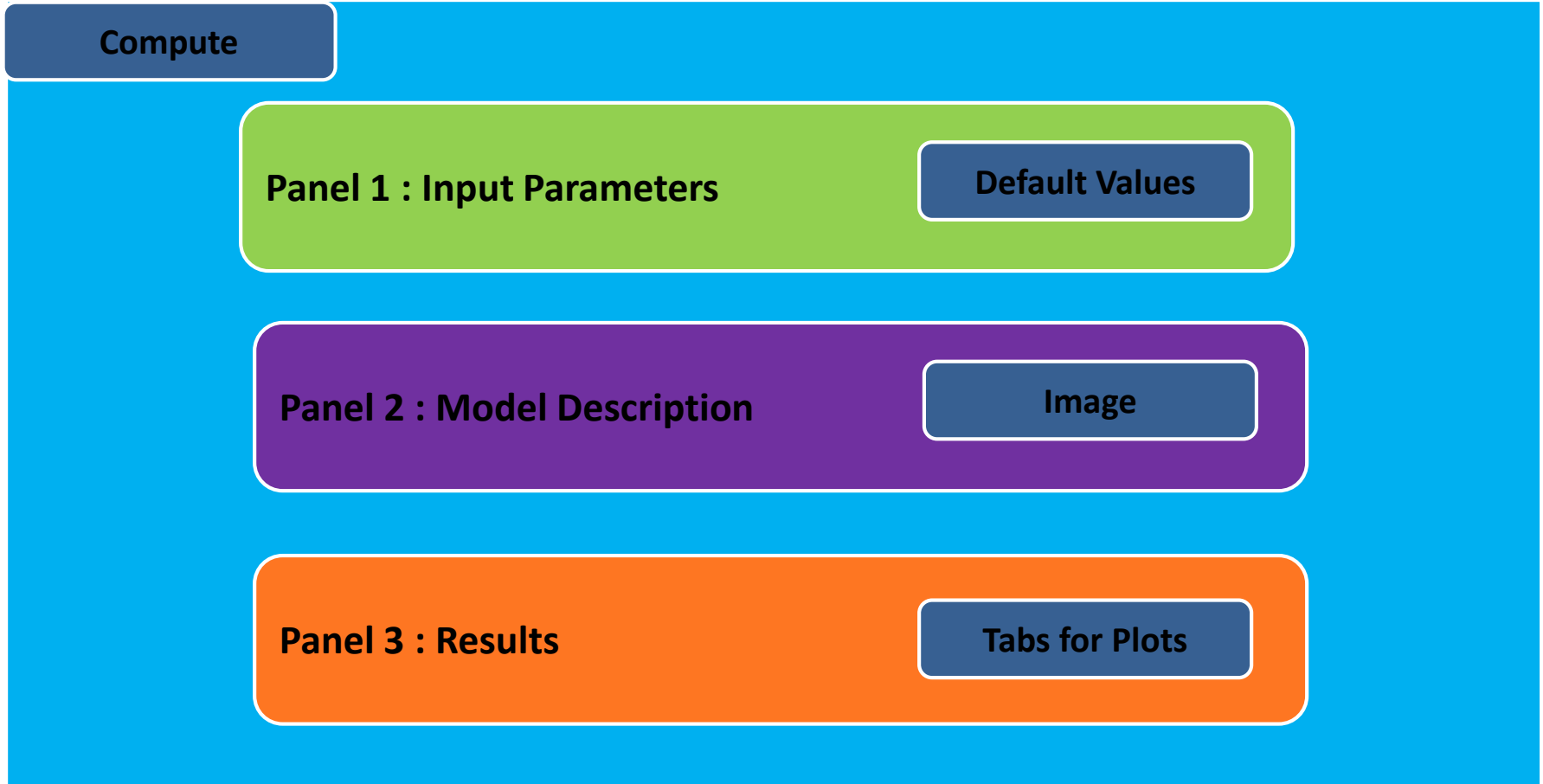
COMSOL Multiphysics as the Numerical Engine

- Finite Element Method analysis modeling tool
- Equation oriented: Physical systems are described in terms of governing microscopic forms of transport laws
- Predefined equations (“Application modes”) are available covering a wide range of physics/multiphysics
- User-defined equations can be added for post calculations
- Modules: Optional application-specific add-ons
- Complete Modeling Package provides:
 - Integrated tools for import of 2D or 3D CAD drawings
 - Automatic or user-controlled meshing of subdomains
 - State-of-the-art solvers for resulting systems of equations
 - Postprocessing / Data Import / Export Capabilities

Steps Involved in GUI Creation



Example of Typical GUI Layout



Catalytic Wall Microreactor Results

Catalytic Wall Reactor

Input

Parameter	Value	Units
Rate Constant	1.5	1/s
Diffusion Coefficient of A	1e-7	m ² /s
Diffusion Coefficient of B	0.5e-7	m ² /s
Concentration of A	1	mol/m ³
Concentration of B	0	mol/m ³
Density	1e3	kg/m ³
Dynamic Viscosity	1e-3	kg/(m*s)
Inlet Pressure	0.1	Pa
Outlet Pressure	0	Pa

Reactor Description

Inlet: A → **Catalytic Wall** (A → B) → Outlet: A, B

Model Description

COMSOL MULTIPHYSICS

Velocity Pressure Concentration of Specie A Concentration of Specie B **Tabs**

Input

Results Panel

COMSOL MULTIPHYSICS

Catalytic Wall Reactor

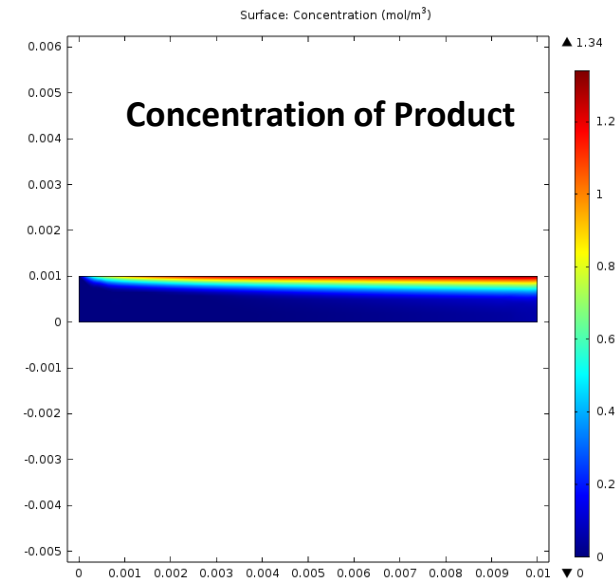
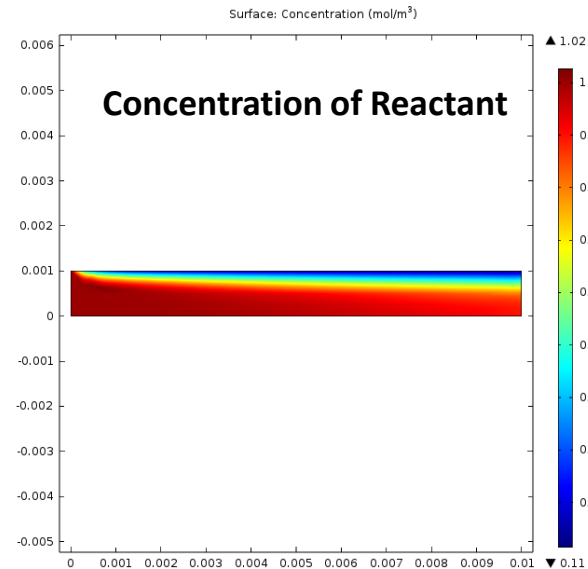
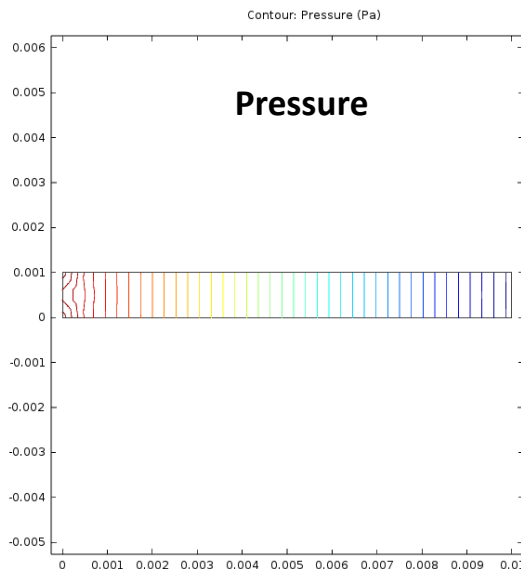
Input

Parameter	Value	Units
Rate Constant	1.5	1/s
Diffusion Coefficient of A	1e-7	m ² /s
Diffusion Coefficient of B	0.5e-7	m ² /s
Concentration of A	1	mol/m ³
Concentration of B	0	mol/m ³
Density	1e3	kg/m ³
Dynamic Viscosity	1e-3	kg/(m*s)
Inlet Pressure	0.1	Pa
Outlet Pressure	0	Pa

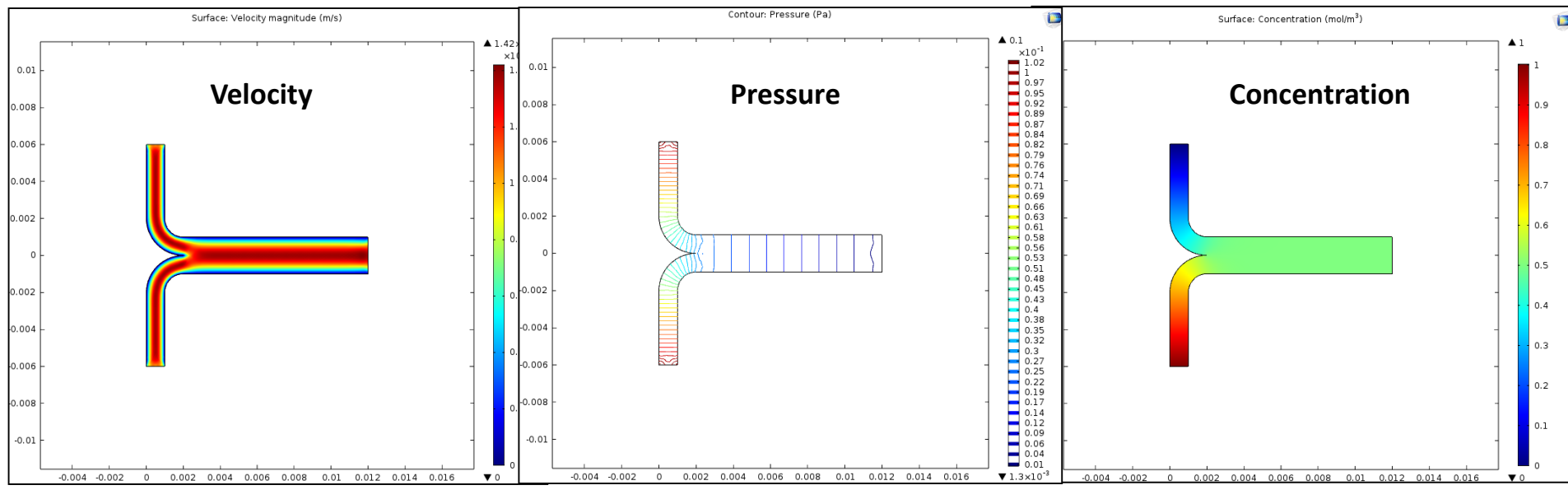
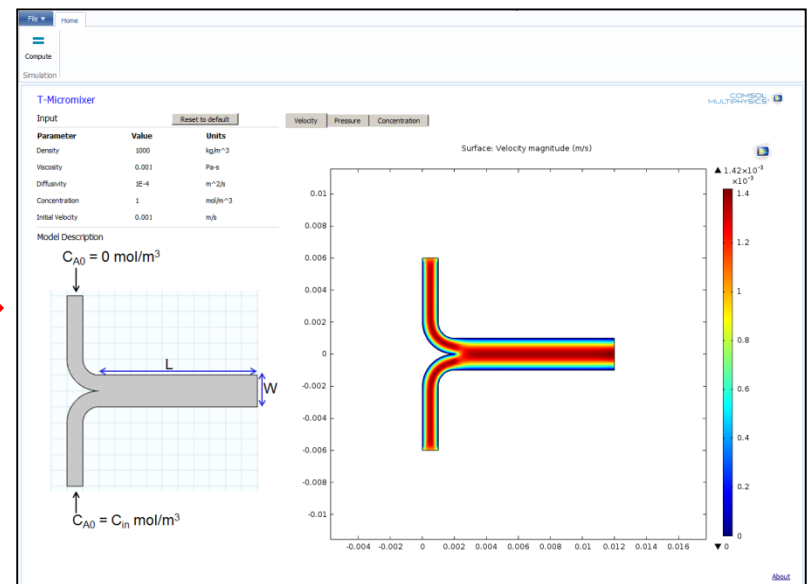
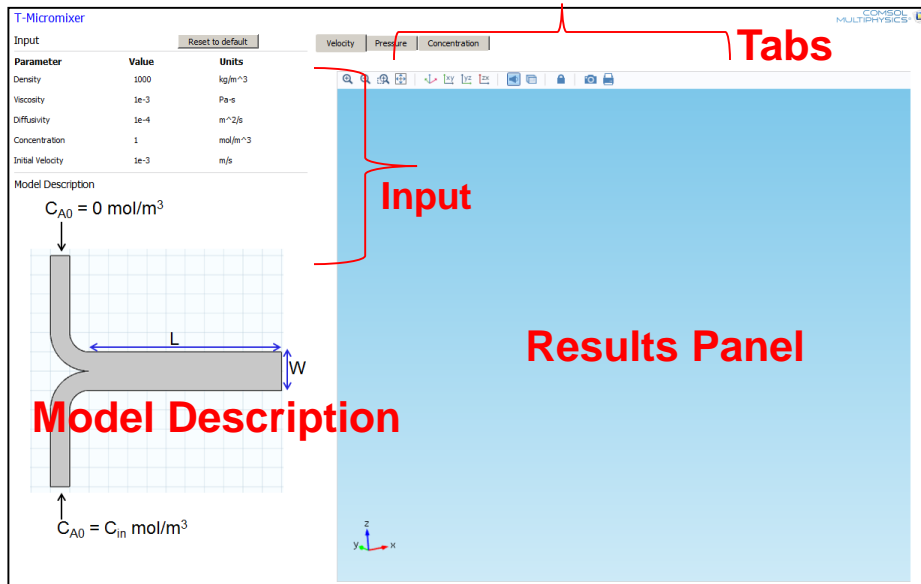
Reactor Description

Inlet: A → **Catalytic Wall** (A → B) → Outlet: A, B

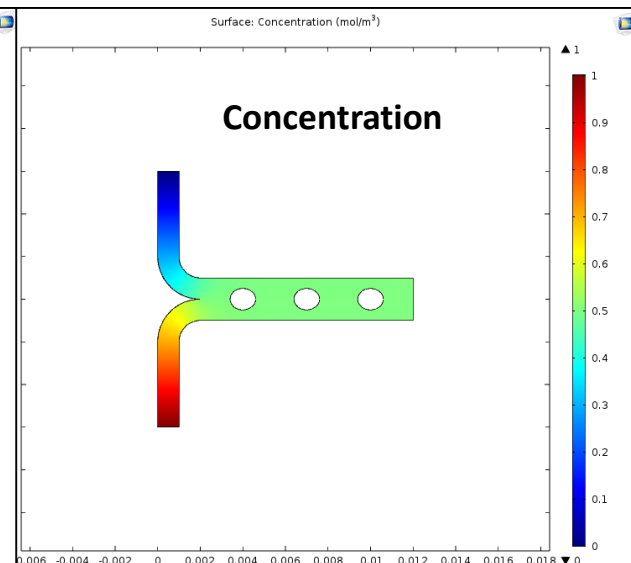
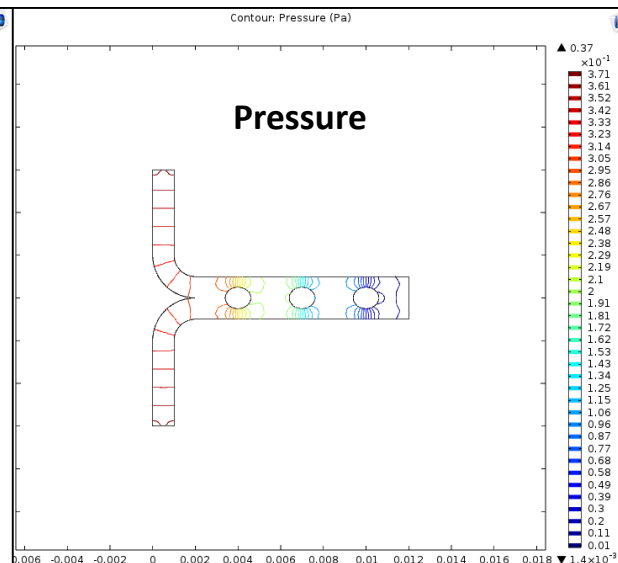
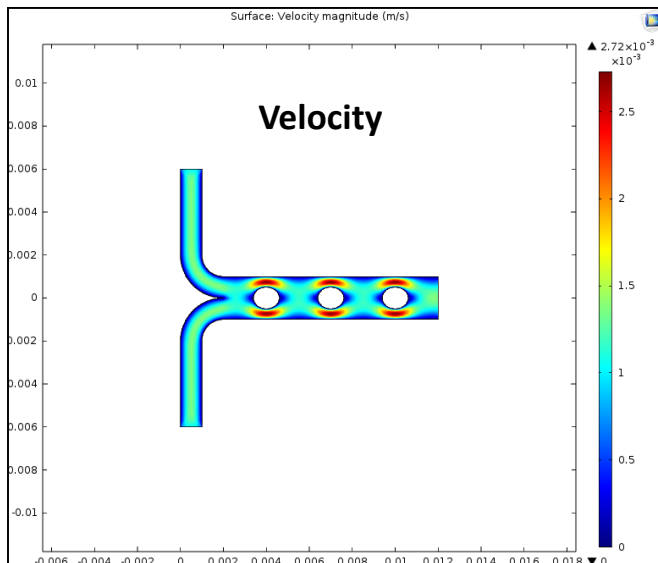
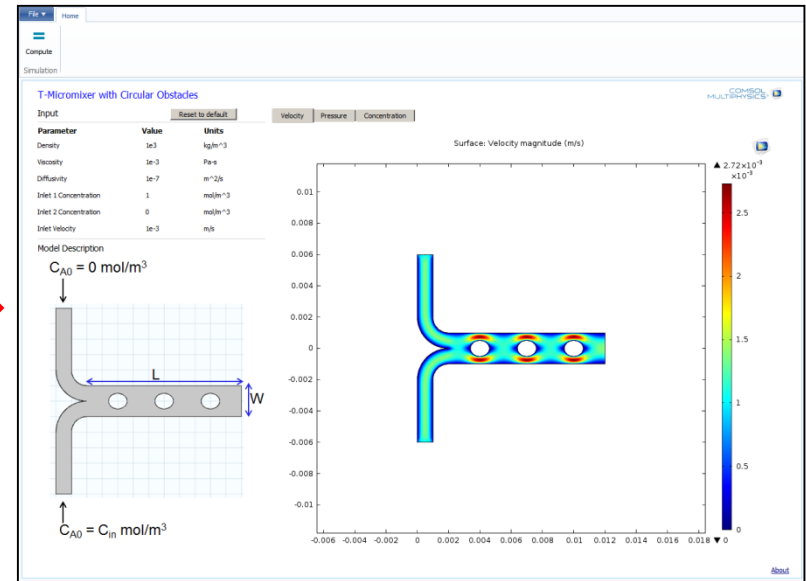
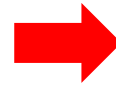
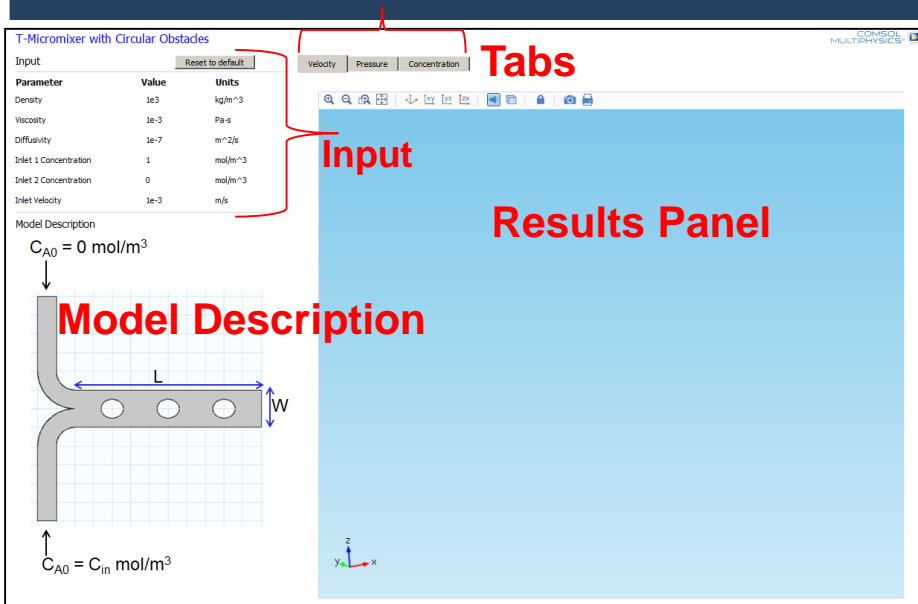
Surface: Velocity magnitude (m/s)



Regular T-Micromixer



T-Micromixer with Circular Baffles



T-Micromixer with Rectangular Baffles

